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# INTERNATIONAL JOURNAL OF ENGINEERING SCIENCES & RESEARCH TECHNOLOGY

# OPTIMIZATION OF CONTROLLER PARAMETER BASED ON TAGUCHI –MPSO APPROACH TO CONTROL NONLINEAR SYSTEM

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**DOI**: 10.5281/zenodo.1199376

# ABSTRACT

In this research work proposed MPSO methods for nonlinear complex processes. These processes are implemented in various process control industries, Design and development of new controller to increase the better stability and improve the performance index. This paper goal the minimize parameters for process controller by Taguchi method combined mutation particle swarm optimization algorithm for industrial laboratory highly complex nonlinear QTS. Analysis of means techniques analyses the meaning of means which are effectively different from the output responses combined means to detect nearer values of PID controller parameters while ANOVA method determines the two most effective parameters with the response of Quadruple tanks system. The result shows that TMPSO technique is provided the good result when compared with other approaches. The TMPSO techniques use for setting controller offers enhanced process specification such as better time domain specifications, smooth error reference tracking, remove the coupling effect and minimization of error in the nonlinear system.

Keywords: Mutation- Particle Swarm Optimization, Nonlinear system, Performance Index.

#### I. INTRODUCTION

In various real-time chemical and petrochemical plants such as spherical tank system Continuous Stirred Tank Reactor (CSTR), other various chemical reactor processes are more nonlinear by characteristics and highly complex in nature. In various process industries, Controller tuning to stabilize these nonlinear multivariable processes and contribute necessary disturbance rejection is the big problem because of their nonlinearity and uncertain phenomena. Most of the processes indicate stable and/or unstable characteristics. Based on the operating condition. In the almost industry process control system essential requirement for proper tuned PID controller for every process. In various literatures of control and nonlinear system, various controllers designing for critical processes are available to stabilize processes [1–5]. Researchers help to tune parameter of PID to control systems by using various techniques to change system better response [1]. It is very simple conception of the controller for a stable operating region, but it's very difficult for nonlinear unstable system, there available increasing and decreeing of controller constant value, and some specific value to be viewed to conception of the controller for the complex system. These nonlinear indicate overshoot and inverse output due to system characteristics [4].

In the recent advanced research on control techniques for process industry such as adaptive control techniques, predictive control, IMC control techniques, soft computing techniques, and conventional controllers are contributing in various process control application reason of their method very simple and robust in nature, also easier to validate [2]. Several years before, in the several manufacturing processes parameter design using particle swarm optimization [14] instead of its requirement for the process of extrusion to design was not better. For the reason that study, they did design on the reduce mandrel eccentricity and output tube bending positions of a billet inside multi-hole extrusion optimization. This research access produce the optimize



# ISSN: 2277-9655 Impact Factor: 5.164 CODEN: IJESS7

responses with respect to the specific operation variable range on basis of the finding knowledge of the results through the very advanced procedure to again enhance the perfect solution of qualities. Hsiang and Lin analytical thought the gist of many operation parameters of the magnesium alloy tubes hot extrusion by using the statistical approach techniques and another analysis of variance (ANOVA) to improve the better result nature of other different parts. It's involved that temperature, the billet, in extrusion velocity, of heating and temperature of container affect the mechanical characteristics of extruded products.

Diminish costly approximate trails and get the key forces of specific variables to make certain best quality [17]. Required best pairs of parameter values of a process by using PSO combine mutation mechanism (MPSO). PSO was assigned random velocity to each and considerable particle due to its search mechanism associates and its own. In this research work, quadruple tank system is laboratory-based highly nonlinear system standard model for an experimentation setup for research as well as practical aspect. Using Taguchi method find the optimized value for PID controller parameter after again this value optimized by MPSO algorithm so that more optimized result we are getting through Taguchi combine with MPSO.

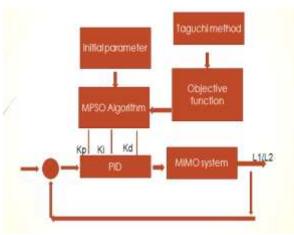


Figure: 1 Block Diagram Taguchi based MPSO for MIMO System

#### **II.QUADRUPLE TANK SYSTEM**

The process which has nonlinear characteristics has a more interaction with quadruple tank processes, which are touchstone processes used in many industries application. This frame-up is very simple and rugged but still, the system would elaborate concerning multiple variable techniques. The process flow diagram is viewed in Figure 1. The main object has to maintain to the levels Y1 and Y2 at bottom tanks with prime movers. This mathematical model needed for the present practical lab includes and also the disturbing effect of flows in and out of the upper-level tanks. Inputs voltage is applied to prime movers voltage V1 and voltage V2. This process is represented by the differential equations according to the material balance equation. Process is represented by equations

Here in the QTS infer a mathematical model. A process schematic is shown in Figure 1. Mass balances yield

$$\frac{dh1}{dt} = -\frac{a1}{A1}\sqrt{2gh1} + \frac{a3}{A1}\sqrt{2gh3} + \frac{\gamma 1k1}{A1}v1$$

$$\frac{dh2}{dt} = -\frac{a2}{A2}\sqrt{2gh2} + \frac{a4}{A2}\sqrt{2gh4} + \frac{\gamma 2k2}{A2}v2$$

$$\frac{dh3}{dt} = -\frac{a3}{A3}\sqrt{2gh3} + \frac{(1-\gamma 2)k2}{A3}v2$$

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ISSN: 2277-9655 Impact Factor: 5.164 CODEN: IJESS7

[Pithadiya \* *et al.*, 7(3): March, 2018] IC<sup>TM</sup> Value: 3.00

$$\frac{dh^{4}}{dt} = -\frac{a^{4}}{A^{4}}\sqrt{2gh^{4}} + \frac{(1-\gamma 1)k^{2}}{A^{4}} v1$$

Where A is tank 1,2,3,4 cross-section area of respective tank, a is the outlet hole cross-section area of respective, and water level h. v1and V2 is the voltage given to Pump and the kivi is respective flow rate. The minimum phase and non minimum phase parameters  $\gamma 1$ ;  $\gamma 2 \in [0; 1]$  are supported by how the valves are in position to on and off for trails.

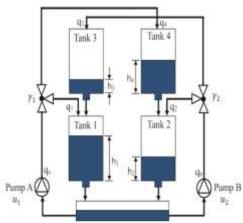


Figure: 2 Quadruple Tank MIMO system

This process presents interacting multiple variable dynamics; complex system because of each of the prime movers involves both of the outputs. This process exhibits nonlinear model and the nonlinear model convert to a linear model of the quadruple-four tank process has multivariable zero, which are to be situated in the left or the right half - s plane by adjusting the throttle valves position  $\gamma 1$  and  $\gamma 2$ . It's showed that the reverse response (non-minimum phase) will happen when the value of this valve in the range of  $0 < \gamma 1 + \gamma 2 < 1$  and minimum phase for  $1 < \gamma + \gamma 2 \leq 2$ . The setting of the valve will be given to the whole overall system dissimilar characteristics from a multiple variable control point of view. Immeasurable disturbances can be enforced through forced water out of the main upper tanks and into the main bottom man-made space small tank. It has been exhibited reject interference as well as mention covering the point. Using the multiple variable four tank process different aspects of multiple variable control systems can be illustrated. Using this algorithm we are getting the good result and improve the performance index ISE and IAE goes minimum. Now all-over system performance increase and index of stability also minimize. For example:

- Development and analysis of decoupling compensator.
- Development and analysis of state feedback compensator for different locations of the zeros.
- The valve settings effect on the location of the zeros.
- Recognize when a process is easy or not to control
- Design and evaluation of decentralized control.
- Development and analysis of mathematical model based predictive Strategy. Development and analysis of μ-analysis-based H∞ control.
- The locations of the zeros on the process output effect in different input directions

# **III.TAGUCHI METHOD (ANOVA)**

The Taguchi method provides a very long meaning of explaining of the separate and mix results of different design principles based on the lowest number of trials (Al-Arifi et al., 2011) Taguchi approach for design variables is available in several categories as a result of an output of every variable to quality characteristics. The different levels of the process outcome are converts into s/n ratio. The standard ratio of signal to Signal to noise basically utilized are as follows: first is the Smaller value the Better, Second the Nominal value the Better, and third is the Higher value -The Better. This research study uses the ratio of Signal to Noise of the ISE and IAE performance to minimize the better stability of the nonlinear quadruple tank system process. The Signal to Noise ratio the Smaller-The Better (STB), characteristics is as follows (Lin and Chou, 2010):



 $\frac{s}{N} = -\log\left(\frac{1}{n}\sum vi^2\right)$ 

Where, n is the number of counts under the same design parameters, yi indicates the measured results and i presents the number of application based variables in the Taguchi OA. An output of S/N ratio figure of paramater levels indicates a better concept with preferable quality within the specified values. The ANOVA techniques utilized for in the Taguchi is a novel statistical approach first excepted to an analysis of the major values of application parameters and also the output of each variable, yi denoted the measured output results and i denotes the number of application parameters available with the Taguchi Orthogonal Array due to ratio of signal and noise, Effect of the Process parameter obtain based on ANOVA. The output of S/N ratio diagram of variable values shows a application with considerable prime within the specified value of variables.

### IV. MUTATION COMBINED WITH PARTICLE SWARM OPTIMIZATION

5

The roots of PSO were instigated through the social behavior of fish schooling or bird flocking. Eberhart and Kennedy counseled the particle swarm computer program optimization pso methodology in 1995. In the search space indicates a good performance for each particle to the minimization specific task and representing as a bunch of different specific variables. This is linked with two path which name is the positioning and velocity path, which called name is the position and acceleration vectors In nth -dimensional search space, the two vectors associated with each particle i are Xi = (xi, 1, xi, 2, ..., xi, n) and Vi = (vi, 1, vi, 2, ..., vi, n), respectively. Every particle changes the levels its result will depend on it is own good survey and the good swarm overall involvement to search it is good fitness level using iterative changing. Moving ahead this iteration process, the change of position and velocity of each and every particle are evaluated as shown in the equation. The global best position and acceleration are change after each iteration value. Equation suggests the updated design variables after mutation of each up to date particle from previous equation. The proposed algorithms were designed to continuous change parameter in specified equation for specific method up to reach termination states.

#### Flowchart of the Taguchi based MPSO techniques

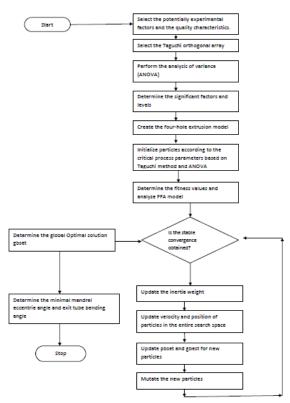


Figure :3 Flow chart Mutation PSO algorithm



[Pithadiya \* et al., 7(3): March, 2018]

ICTM Value: 3.00

11

ISSN: 2277-9655 Impact Factor: 5.164 CODEN: IJESS7

# V. SIMULATION RESULT AND DISCUSSION

# Taguchi and ANOVA

Using Mutation based PSO we can also optimize again for the value from the Taguchi method So that we can more optimized value for the parameter of PID and getting good response for nonlinear system Result for Taguchi with MPSO KP1 = 7, KI1 = 6.9, KP2 = 5.4, KI2 = 9.3

TABLE I: Design variables and Their Coded Levels							
Tuning constant	stage 1	stage 2	stage				
			3				
Kp1	10	11	12				
Ki1	7	8	9				
Kp2	11	12	13				
Ki2	8	9	10				

TABLE I: Design	Variables a	nd Their	Coded Levels
INDEL I. DUSIEN	<i>i</i> un nuones u	nu incn	Coucu Levens

#### **Orthogonal Array**

# TABLE II: DESIGN VARIABLES and THEIR CODED LEVELS

Ex p.	Kp1	Ki1	Kp2	Ki2	ISE1	ISE2	E^2	S/N
1	1(10)	1(7)	1(11 )	1(8)	4.9889E -03	5.267 8E-03	5.2639E -05	50.3381 9
2	1(10)	2(8)	1(11 )	2(9)	2.4900E -02	2.550 0E-02	1.2703E -03	36.6296 5
3	1(10)	3(9)	1(11 )	3(10 )	5.3089E -02	6.375 9E-02	6.8837E -03	28.6300 5
4	1(10)	2(8)	2(12 )	1(8)	1.9877E -02	2.580 4E-02	1.0609E -03	36.5301 4
5	1(10)	3(9)	2(12 )	2(9)	5.3474E -02	6.422 9E-02	6.9848E -03	28.5655 3
6	1(10)	1(7)	2(12 )	3(10 )	4.1322E -03	4.420 9E-03	3.6619E -05	51.8607
7	1(10)	3(9)	3(13 )	1(8)	6.0211E -02	6.445 6E-02	7.7799E -03	28.5231 3
8	1(10)	1(7)	3(13 )	2(9)	3.6644E -03	4.426 1E-03	3.3018E -05	51.8505 5
9	1(10)	2(8)	3(13 )	3(10 )	2.0020E -02	2.536 8E-02	1.0443E -03	36.6781 3
10	2(11)	2(8)	1(11 )	1(8)	1.1220E -04	1.782 0E-03	3.1881E -06	59.7530 4
11	2(11)	3(9)	1(11 )	2(9)	1.0111E -02	1.016 7E-02	2.0560E -04	44.6255 8
12	2(11)	1(7)	1(11 )	3(10 )	7.2311E -06	8.235 1E-06	1.2011E -10	106.457 8
13	2(11)	3(9)	2(12 )	1(8)	2.0000E -07	1.003 9E-02	1.0078E -04	44.7369 7
14	2(11)	1(7)	2(12 )	2(9)	1.2100E -04	1.003 3E-02	1.0068E -04	44.7421 6
15	2(11)	2(8)	2(12 )	3(10 )	1.2121E -03	1.788 4E-03	4.6676E -06	59.7218 9
16	2(11)	1(7)	3(13 )	1(8)	2.1313E -05	2.348 2E-05	1.0056E -09	97.3565 1
17	2(11)	2(8)	3(13 )	2(9)	1.3264E -03	1.791 8E-03	4.9699E -06	59.7053 9

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2(11)	3(9)	3(13	3(10				44.6346
```	- (- /	)	)	-04	8E-02	-04	
3(12)	3(9)	1(11	1(8)	3.1216E	4.705	2.2243E	71.3183
J(12)	5(7)	)	1(0)	-05	9E-04	-07	6
2(12)	1(7)	1(11	2(0)	3.1216E	4.705	2.2243E	#NUM!
5(12)	I(I)	)	2(9)	-05	9E-04	-07	#INUIVI !
2(12)	2(0)	1(11	3(10	5.2164E	5.901	2.7559E	129.351
5(12)	2(8)	)	)	-06	9E-07	-11	4
2(12)	1(7)	2(12	1(0)	3.2515E	4.352	1.9046E	
3(12)	1(7)	)	1(8)	-05	1E-04	-07	#NUM!
2(12)		2(12		1.4550E	1.788	3.2199E	119.721
5(12)	2(8)	)	2(9)	-07	5E-06	-12	4
2(12)	2(0)	2(12	3(10	3.2154E	4.573	2.1017E	71 5 (7
3(12)	3(9)	)	)	-05	1E-04	-07	71.567
2(12)		3(13	1(0)	1.6432E	1.815	5.9947E	139.593
3(12)	2(8)	)	1(8)	-07	1E-07	-14	2
2(12)	2(0)	3(13	2	3.2515E	4.352	1.9046E	71.9972
5(12)	3(9)	)	2(9)	-05	1E-04	-07	3
2(12)	1(7)	3(13	3(10	1.6432E	1.815	5.9947E	
3(12)	1(/)	)	)	-07	1E-07	-14	#NUM!
	2(11) 3(12) 3(12) 3(12) 3(12) 3(12) 3(12) 3(12) 3(12) 3(12)	3(12)       3(9)         3(12)       1(7)         3(12)       2(8)         3(12)       1(7)         3(12)       1(7)         3(12)       2(8)         3(12)       3(9)         3(12)       2(8)         3(12)       2(8)         3(12)       3(9)         3(12)       3(9)	$\begin{array}{c ccccc} 2(11) & 3(9) \\ \hline \\ 2(11) & 3(9) \\ \hline \\ 3(12) & 3(9) \\ \hline \\ 3(12) & 1(7) \\ \hline \\ 3(12) & 2(8) \\ \hline \\ 3(12) \\ 3(12) \\ \hline \\ 3(13) \\ \hline \\ \\ \\ 3(13) \\ \hline \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ $	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\begin{array}{c c c c c c c c c c c c c c c c c c c $	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$

# **Results of ANOVA**

#### TABLE III: ANOVA method for QTS

Factor	S1	S2	S3	DOF	Sum of Squares		Factor Effect (percent)
KP1	10	11	12	2	307	153	45
KI1	7	8	9	2	95	47	14
KP2	11	12	13	2	259	130	38
KI2	8	9	10	2	14	7	2

#### Result Comparison of GA and MPSO PID controller performance time domain specification

Controller	Para meter	Minimum phase		Non minimum phase	
		Lev 1	Lev 2	Lev 1	Lev 2
	Settling time	5	5.5	20	700
	Peak overshoot	1	2	30	20
	Rise time	12	12	39	32

# TABLE IV: Comparison Taguchi based GA and MPSO for QTS

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**ISSN: 2277-9655** 



PID with Taguchi	Settling time	5	5.5	22	700	
based						
MPSO	Peak overshoot	1	2	30	20	
	Rise time	7.5	4.5	20.5	120	

### **Performance Index Specification**

TABLE V:	Comparison Per	formance Index Tag	uchi based GA and MPSC	) for QTS
	N ( 1 1	T 11(1 11(1)	T = 10(1 + 1(0))	

Methods	Tank I (height I)		Tank2 (height 2)	
	ISE	IAE	ISE	IAE
PID Taguchi based GA	12	2.35	15.6	5.6
PID Taguchi based MPSO	10.02	5.5	8.38	3.5

### VI. CONCLUSION

This research paper presented for finding the best optimal solution for the nonlinear dynamic system. These techniques to find optimize the parameter of the controller for multiple inputs and multiple output dynamic system using Taguchi statistical method based on MPSO techniques.

This method utilized to find optimal parameter Kp, Ki, and Kd of PID controller based on the performance index to increase the stability and performance of the dynamic nonlinear mimo system. By using the orthogonal array and ANOVA in Taguchi method based on a signal to noise ratio determine the level of the parameter of quadruple tank system based on performance index ISE and IAE. Taguchi based MPSO techniques could be utilized for the better response than Taguchi based in GA for quadruple tank system. These techniques to search optimal value from Taguchi method after that again Taguchi combine with MPSO with the better optimal value of controller parameter. That parameter gives the best result and optimized (minimize) performance index. Minimize performance index all over system performance increase. The results indicate that the Taguchi based MPSO methods can act as the best techniques of the mimo nonlinear system and it can be extended to other nonlinear process control parameter for the various industrial process control system.

The effect indicate that the taguchi based MPSO strategies can act as quality strategies of the MIMO nonlinear process and might be extended to different nonlinear method controller parameter for the industrial process control system.

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# ISSN: 2277-9655 Impact Factor: 5.164 CODEN: IJESS7



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ICTM Value: 3.00

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#### **CITE AN ARTICLE**

Pithadiya, P., Prof., Shah, V., Dr, Shah, C., Prof., & Rajyaguru, V. C., Prof. (n.d.). OPTIMIZATION OF CONTROLLER PARAMETER BASED ON TAGUCHI – MPSO APPROACH TO CONTROL NONLINEAR SYSTEM. *INTERNATIONAL JOURNAL OF ENGINEERING SCIENCES* & *RESEARCH TECHNOLOGY*, 7(3), 463-470.

ISSN: 2277-9655 Impact Factor: 5.164 CODEN: IJESS7